

A METHODOLOGY FOR DESIGNING CONTROLLERS FOR INDUSTRIAL SYSTEMS BASED ON NONLINEAR SEPARATION MODEL AND CONTROL

Masatoshi NAKAMURA (Saga University, Japan)

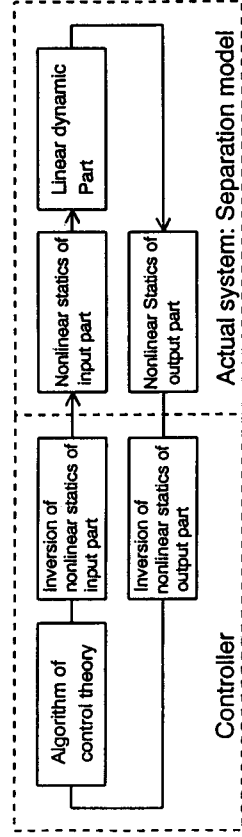
- Controller Design for Industrial Nonlinear Dynamical Systems
 - Nonlinear Separation Model and Control
 - Reduction the Gaps between Theory and Practice

CONTENTS

- Nonlinear Separation Model and Control
- Controller Design
 - Nonlinear Chemical Reactor
 - Tanked Water System
 - Robot Arm

NONLINEAR SEPARATION MODEL AND CONTROL

- Nonlinear Statics and Linear Dynamics



- Controller Design
 - Mirror Image of the Separated Model
 - Nonlinear Statics – Inversion
 - Linear Dynamics – Linear Control

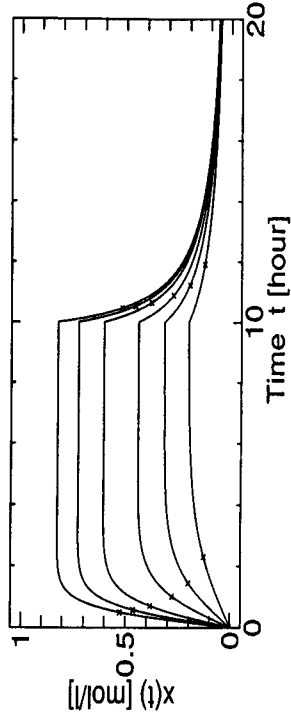
NONLINEAR CHEMICAL REACTOR

- Control Object

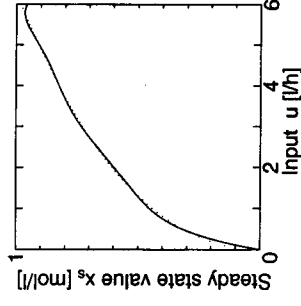
$$\frac{dx(t)}{dt} = -K_r(x(t))^2 + \frac{1}{V}(D_c - x(t))u(t)$$

x : Output Concentration, u : Inflow Rate
 K_r : Reaction Speed, V : Reactor Capacitor
 D_c : Input Concentration

- Follow the Output Concentration x to a Desired Value
- Step Response for $u(0.2, 0.5, 1, 2, 3, 4)$



- Nonlinear Separation Model



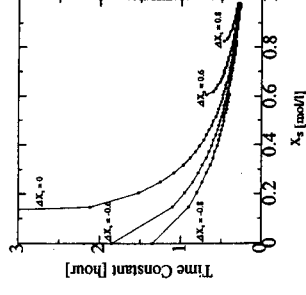
$$G_n(s) = \frac{X(s)}{U(s)} = \frac{X_s(s) X(s)}{U(s) X_s(s)} = \frac{K(u)}{1 + T(x_s, \Delta x_s) s}$$

- Nonlinear Statics

$$x_s = \sum_{i=0}^6 a_i(u)^i$$

- Dynamics

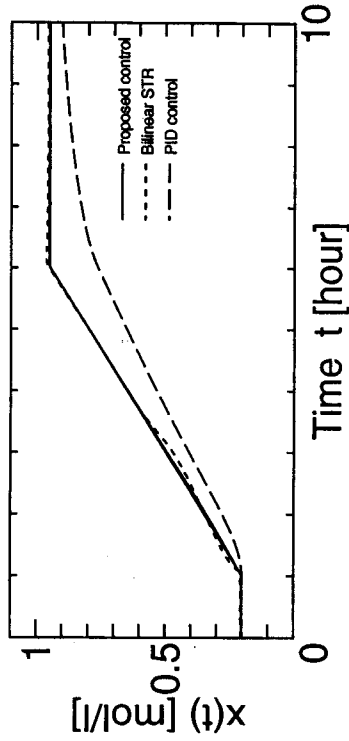
$$G_d(s) = \frac{X(s)}{X_s(s)} = \frac{1}{1 + T(x_s, \Delta x_s) s}$$



○ Controller Design

- Inversion of Nonlinear Statics : $u = \sum_{i=0}^6 b_i(x_s)^i$
- Inverse Dynamics: $G_d^{-1}(s) = 1 + T(x_d, \Delta x_d) s$

○ Simulation Results



○ Nonlinear Separation Model

• Level Meter

Float-Potentio

$$V_{H_m} = 1.66 \times 10^{-3}(H_m)^3 - 7.22 \times 10^{-2}(H_m)^2 + 1.48H_m - 11.5.$$

• Thermometer

$$V_{T_m} = 9.04 \times 10^{-9}(T_m)^3 - 3.01 \times 10^{-3}(T_m)^2 + 3.40 \times 10^{-1}T_m - 7.37.$$

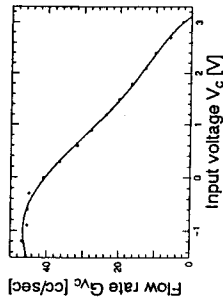
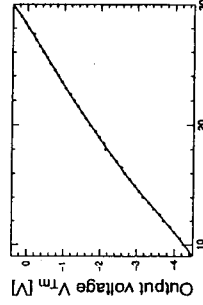
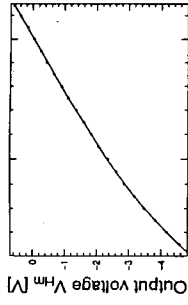
• Actuator

DC Motor-Valve

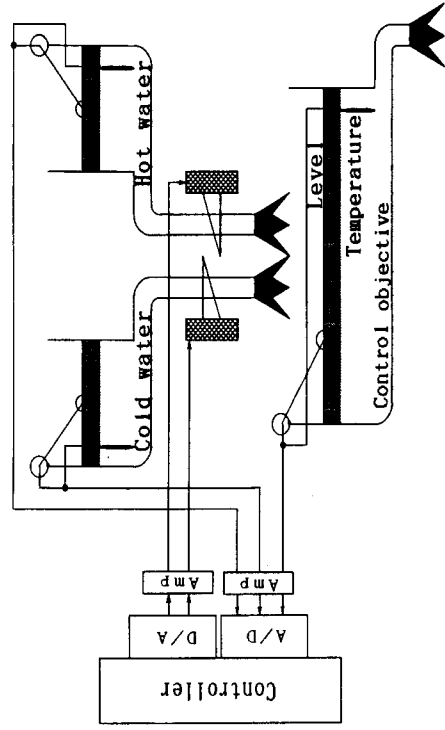
$$G_{V_c}(V_c, H_c^0) = -1.49 \times 10^{-1}(V_c)^5 + 3.50 \times 10^{-1}(V_c)^4 + 1.60(V_c)^3 - 4.35(V_c)^2 - 11.4V_c + 40.7,$$

$$G_{H_c}(V_c, H_c) = -1.68 \times 10^{-4}(H_c)^5 + 3.95 \times 10^{-3}(H_c)^4 + 3.53 \times 10^{-2}(H_c)^3 - 1.69(H_c)^2 + 16.6H_c - 35.7$$

→ Linear Dynamical System



TANKED WATER SYSTEM



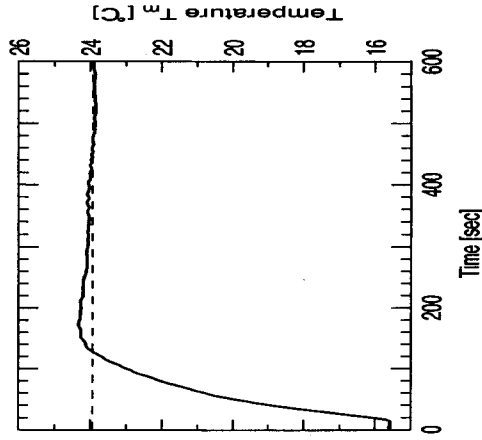
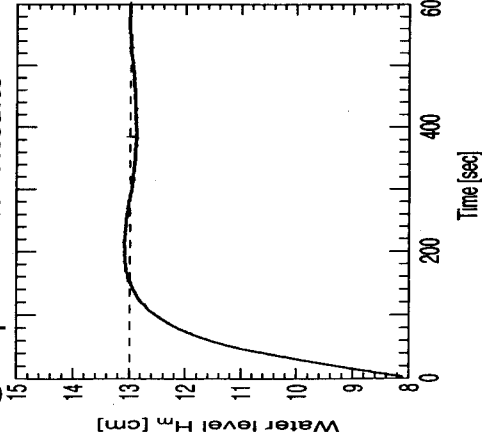
○ Control Objective

Maintain Level and Temperature of Lower Tanked Water at Respective Desired Values

○ Controller Design

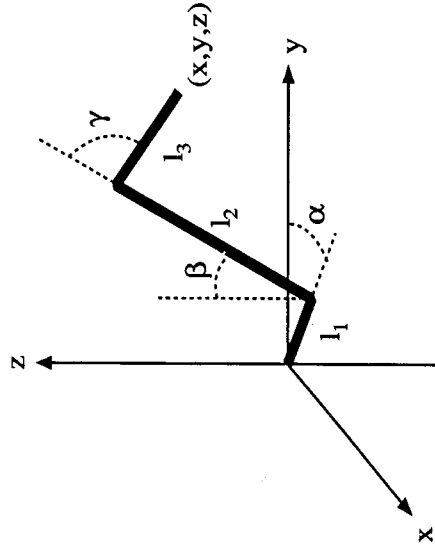
- Inversion of Nonlinear Statics for Detectors and Actuator
- A Delay Compensation Method

○ Experimental Results



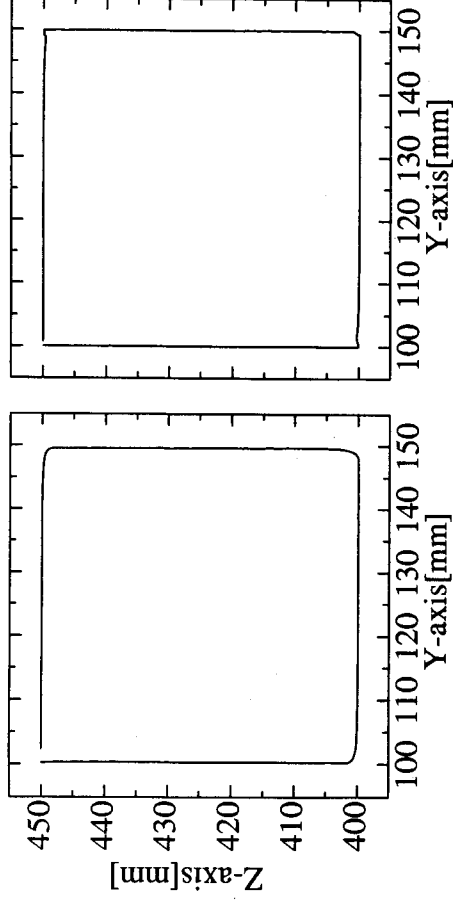
ROBOT ARM

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- Control Objective
Accurate Contour Trajectory of Articulated Robot Arm

- Experimental Results

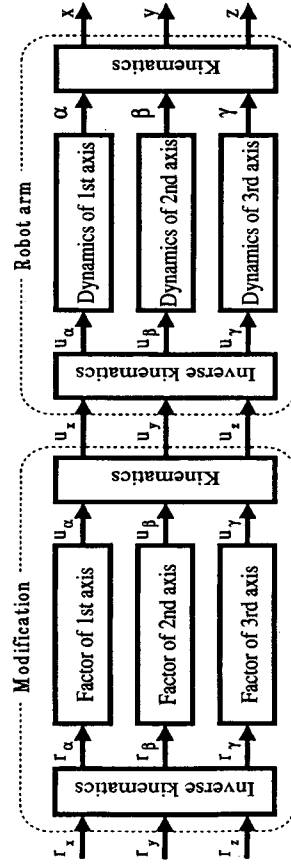


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- Nonlinear Separation Model



- Dynamics of Each Link

$$G(s) = \frac{K_p K_v}{s^2 + K_v s + K_p K_v}$$

- Controller Design
 - Nonlinear Statics – Kinematics, Inverse Kinematics
 - Linear Dynamics – Modified Taught Data Method

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